

BMEGEÁTMW03 „FLOW MEASUREMENTS”

Optical flow visualization,
Introduction to lasers applied to optical flow
diagnostics
Laser-optical measurement techniques for flow
characterization

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AIM:

- VISUALIZATION of the FLOW FIELD
- MEASUREMENT of FLOW VELOCITY $\underline{v}(\underline{r},t)$

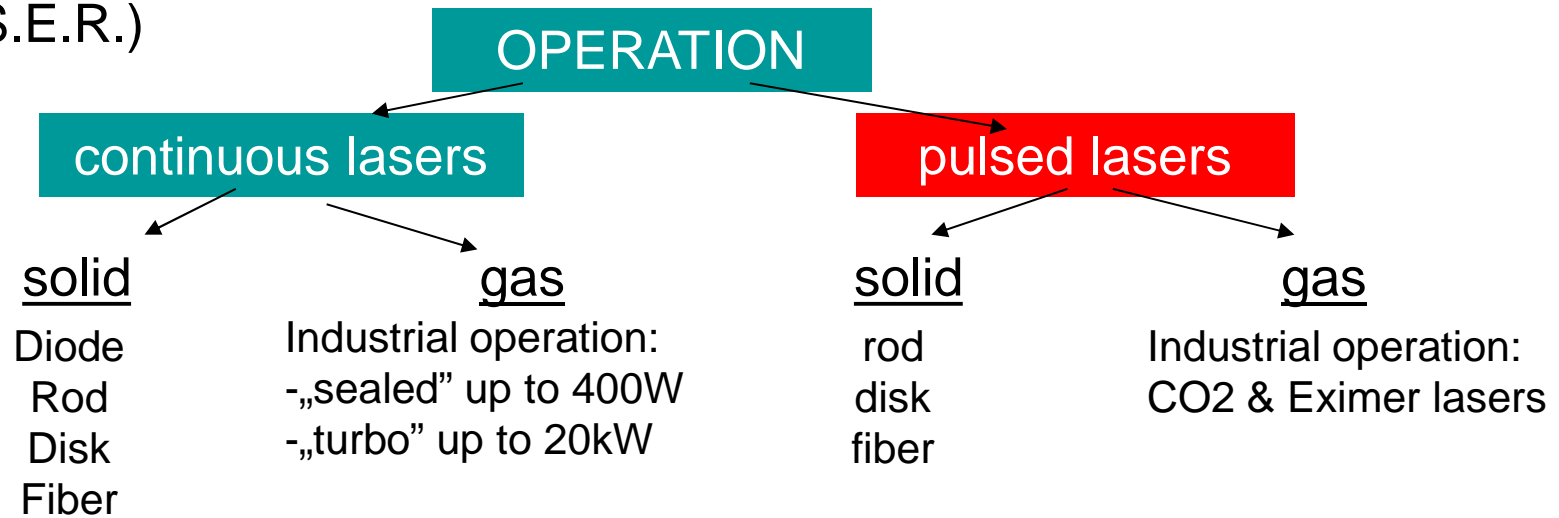
& CHARACTERISATION of PARTICULATE PHASE (d_p)

Contents:

- Lasers, examples (FlowVis, LDV, PDA, PIV, PTV(S))
- Characterization of particle-laden mixtures
- Particle dynamics, equation of motion
- Particles: seeding/tracer problematic

- Advantage / disadvantage / limits of laser-optical techniques

...lasers...
(L.A.S.E.R.)



for LASER OPTICAL FLOW MEASUREMENTS:
from ~10 mW..... to ~6W

FLOW MEAS?

- Flow visualization
- LDV: Laser Doppler Velocimetry
- PDA: Phase Doppler Anemometry

Example:

diode, HeNe, Ar-Ion, Nd:YAG

FLOW MEAS?

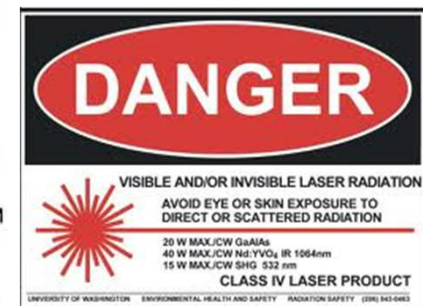
- Flow visualization (!cont.mode)
- PIV: Particle Imaging Velocimetry
- PIV, PTV(S)

Example:

Nd:YAG, CVL (copper-vapour), Ar-Ion, CO2

main „Laser DANGER” signs

EU sign: Class 1, 1M, 2, 2M, 3R, 3B, 4
USA sign: Class I., II., III., IV.)



MEANING of the class signs:

1. : ~ equivalent to sunlight
- 1M. : ~ avoid to examine the light source with optical elements
2. : 400-700nm, max.1mW, cont., up to MPE=0.25s (max permissible exposition time), light protectors are not needed up to this MPE
- 3A,R : up to max. 5mW, cont. operation
- 3B : ! eye protector, safety measures: starting key and beam shutter is a must
4. : ! as all above + direct & undirect reflected lights are also dangerous

Available lasers at the Department or R&D partners:

1) for FLOW VIS:

- laser diodes (10, 25, 50, 100, 500 mW) for flow visualization (610nm, 532nm)

2) Laser Doppler Velocimeters:

2.1 15mW LDV, „ILA” LDV, HeNe: $\lambda=632\text{nm}$ (red), 1D, without Bragg cell (=unshifted)

2.2 300mW LDV Melles Griot, Ar-Ion, $\lambda=514\text{nm}$, 488nm (green, blue), 2D, with Bragg cell

Others, used in R&D cooperation with other institutions:

a) LDV Laser Doppler Velocimeter:

UNI MAGDEBURG 100mW diode „POLYTEC LDV-380” $\lambda=810\text{nm}$ (infrared)

VKI (many, mainly 50-300mW 1D 632nm (red) or 2D

b) Particle Image Velocimeter and Particle Tracking Velocimetry & Sizing

PIV+PTV(S): VKI: Von Kármán Institute (Nd:YAG, 6W, green)

Other PIV-s: from UNI Magdeburg; ELTE – PIV Lab for Atmospheric Flows

c) Phase Doppler Anemometer

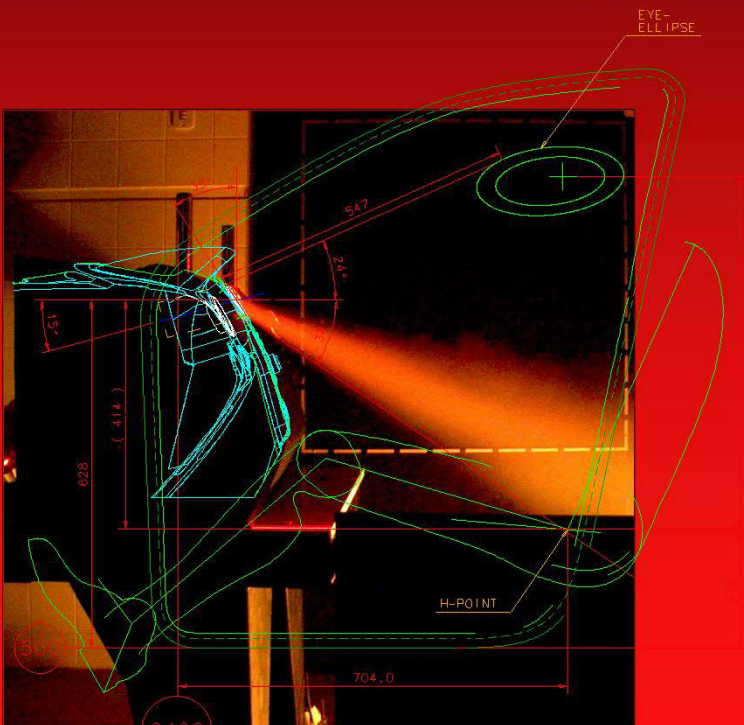
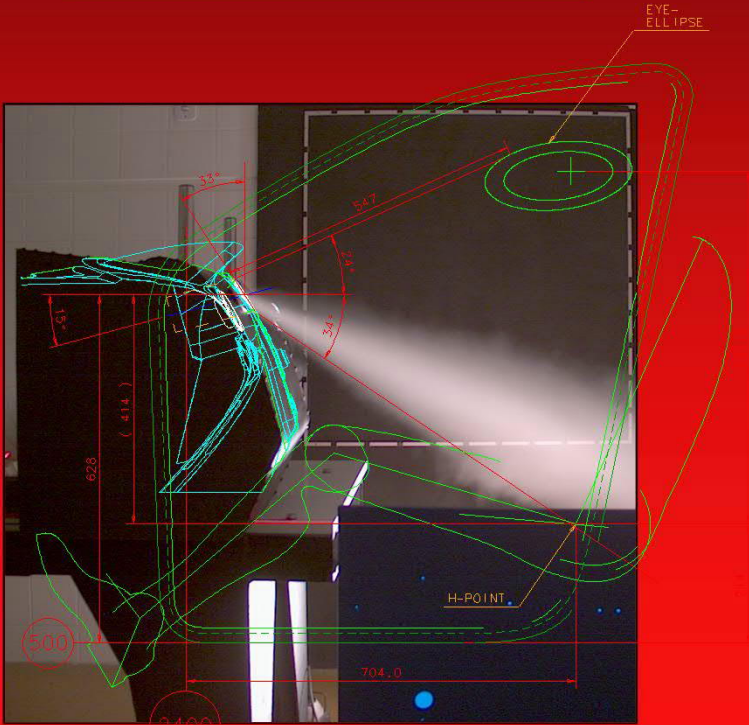
At VKI (Von Kármán Institute) and at UNI Karlsruhe (125mW 632nm)

FLOW VISUALIZATION (50 - 100 mW diode)



light sheet illumination

laser sheet illumination



C.V.3.jpg

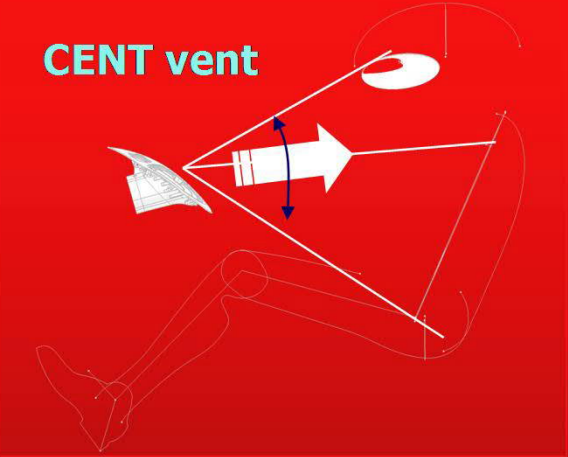
C.V.3_L.jpg

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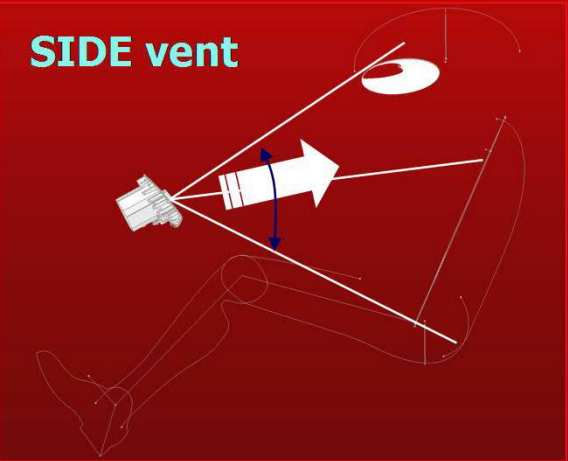
FLOW VISUALIZATION (50 - 100mW diode)

VERTICAL flow distribution

CENT vent

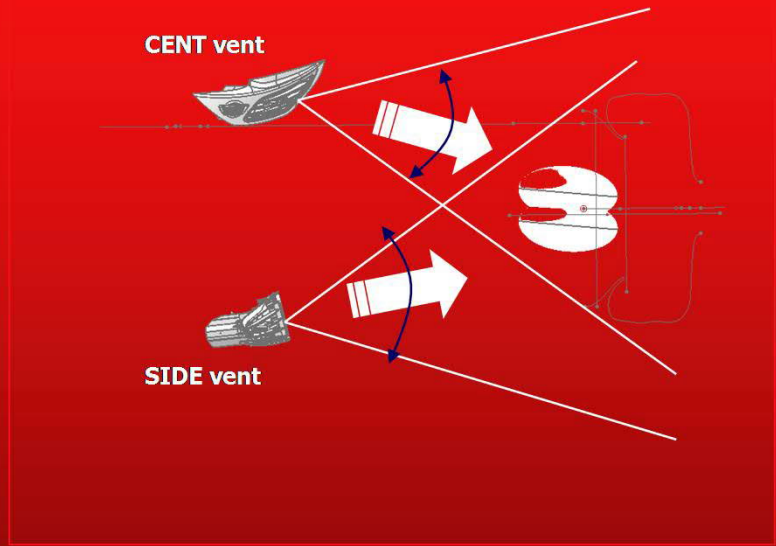


SIDE vent



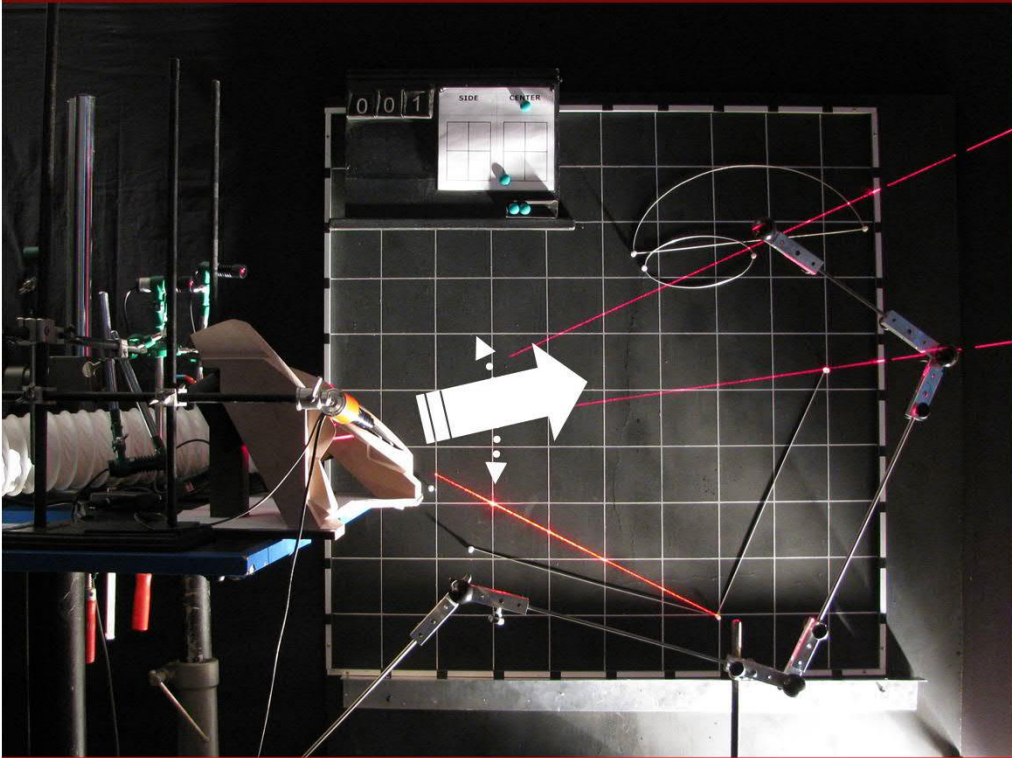
HORIZONTAL, CROSS flow distribution

CENT+SIDE vent



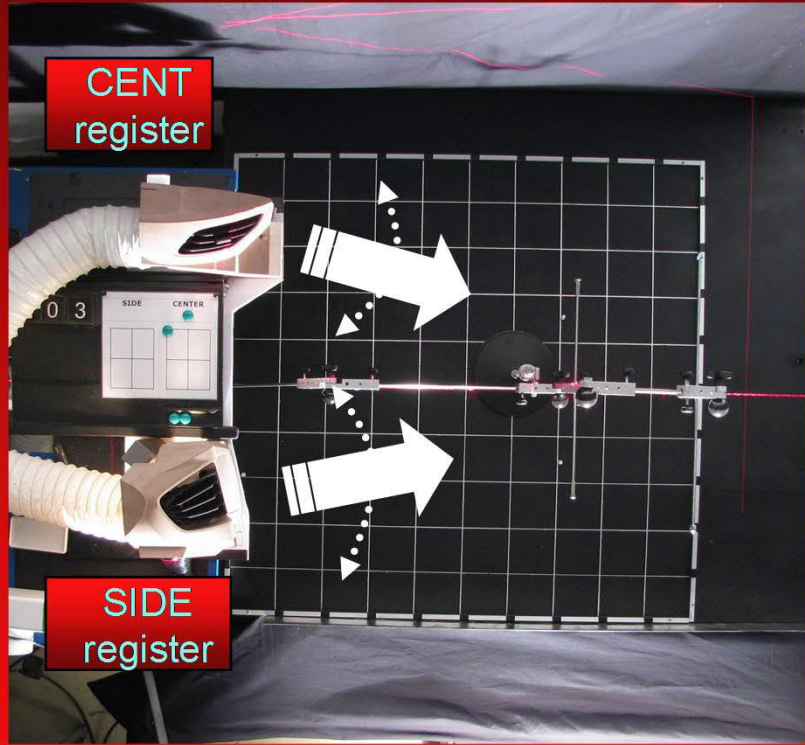
FLOW VISUALIZATION (50 – 100 mW diode)

VERTICAL flow view



side view

HORIZONTAL flow view (SINGLE & CROSS)

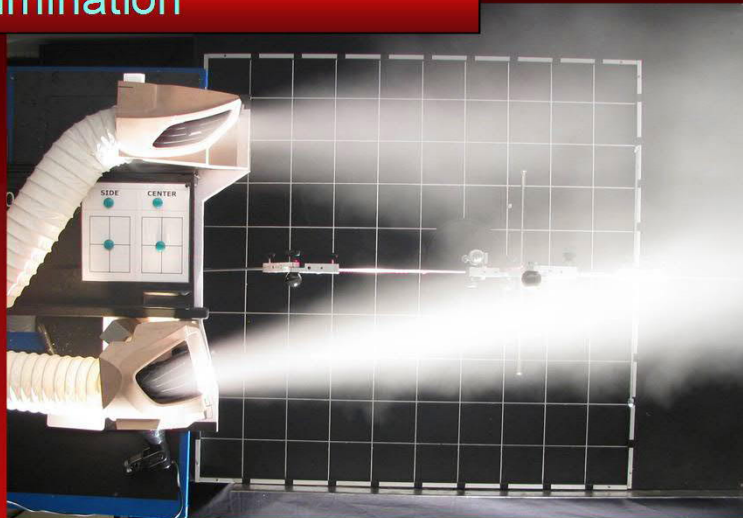


top view

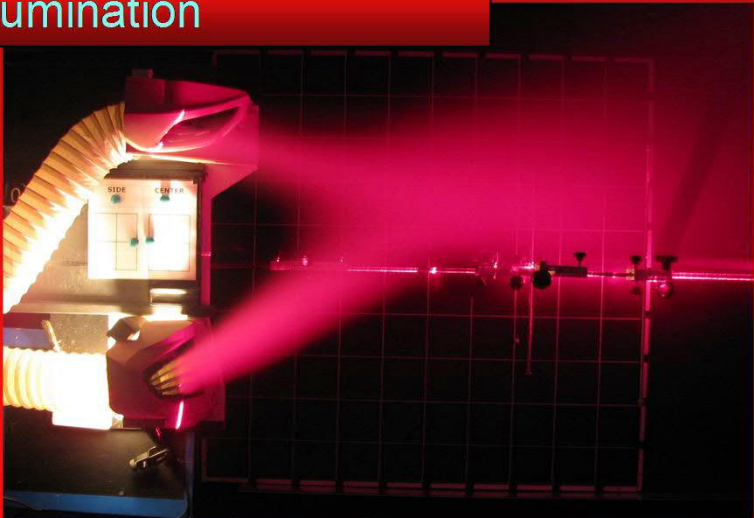
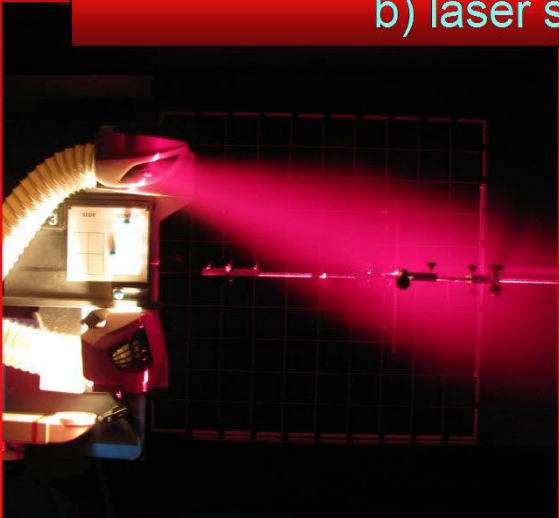
FLOW VISUALIZATION (50 – 100 mW diode)

Two types of illumination are used:

a) light sheet illumination

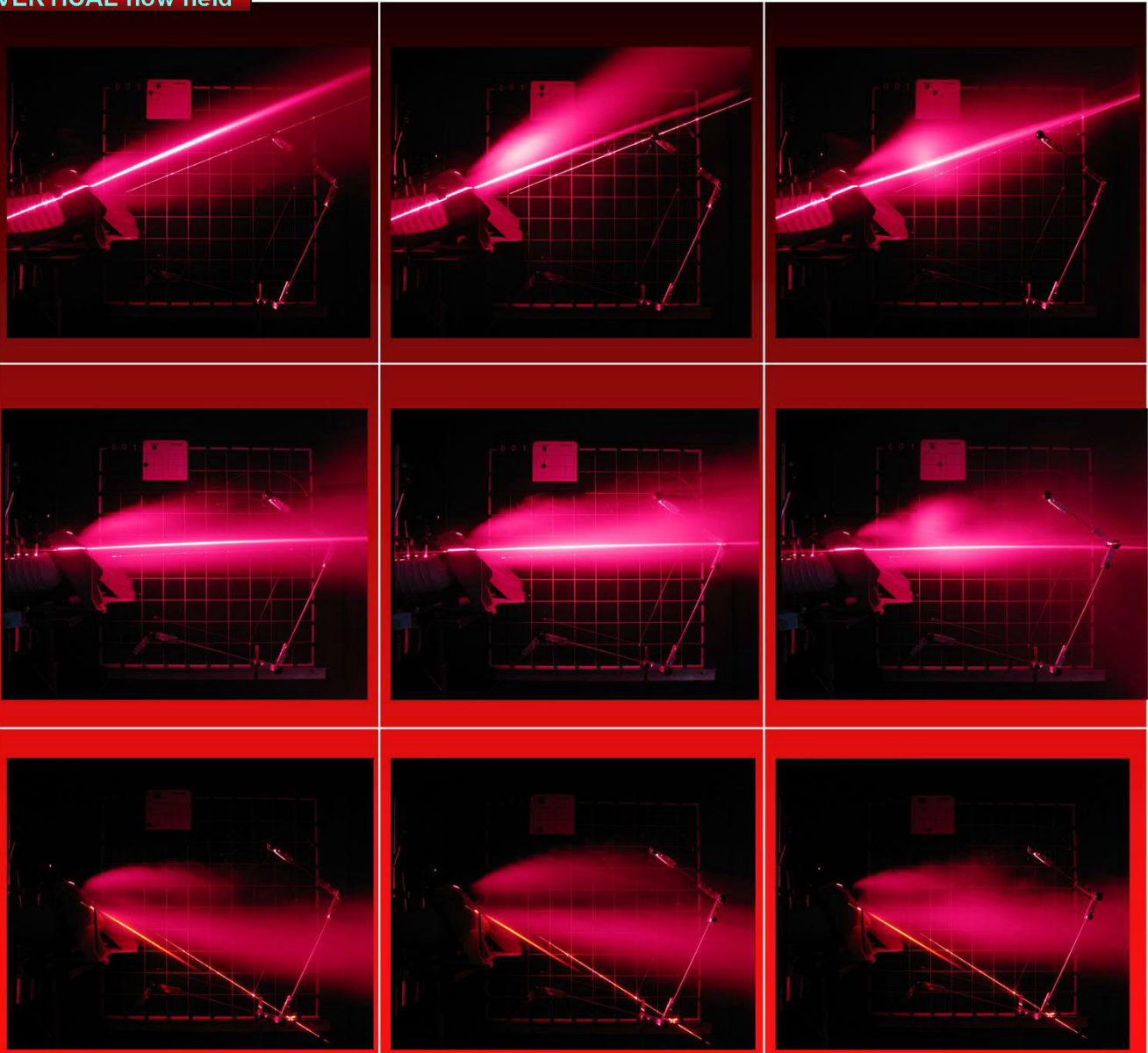


b) laser sheet illumination

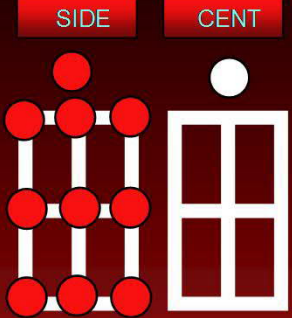


FLOW VISUALIZATION (50 – 100 mW diode)

VERTICAL flow field



SIDE **CENT**



laser sheet illumination

FLOW VISUALIZATION (50 – 100 mW diode)

CROSS flow field

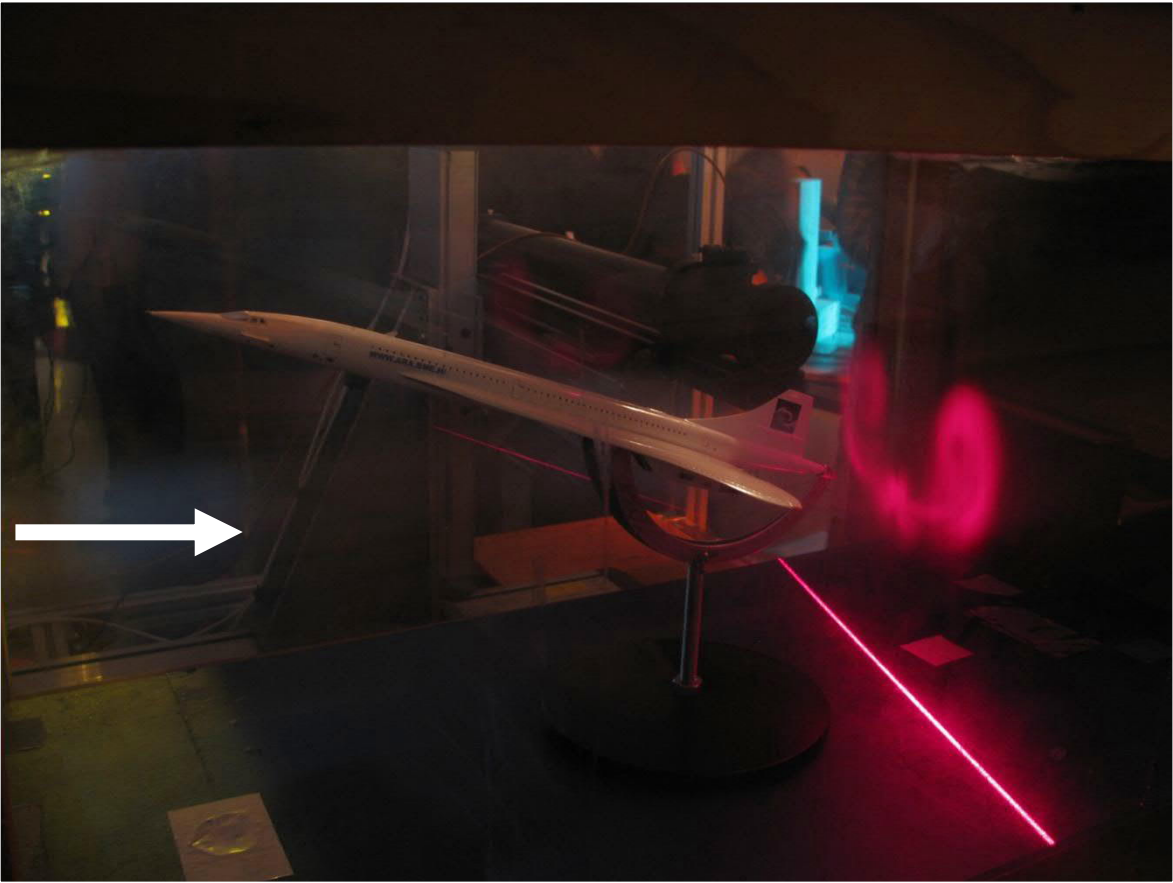
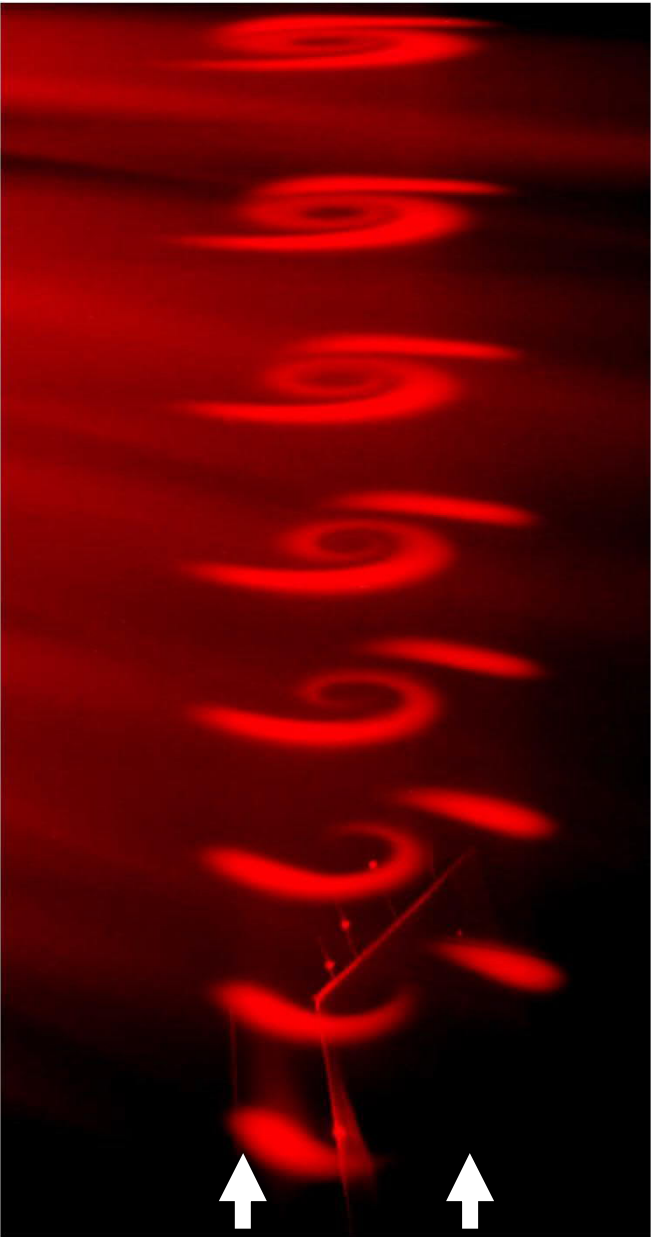


SIDE **CENT**

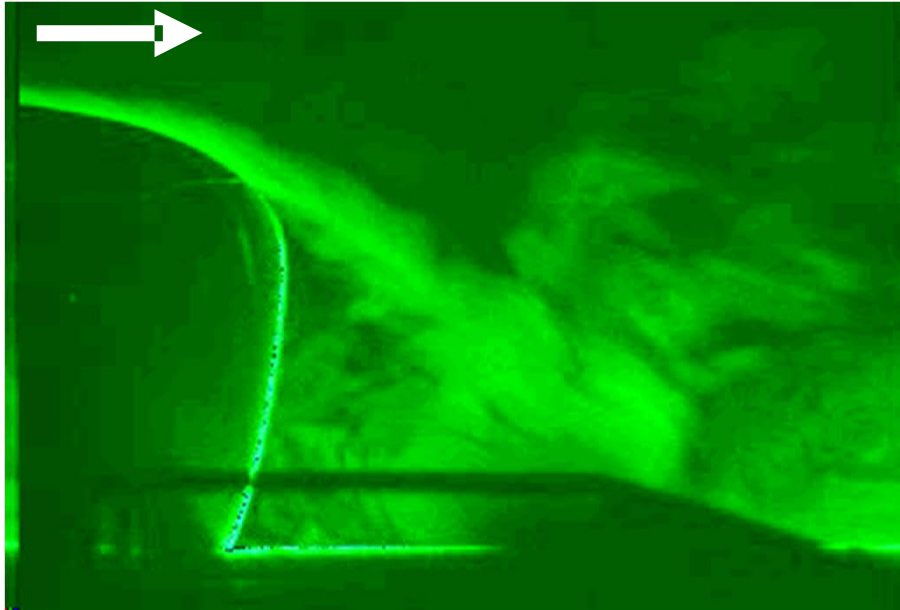
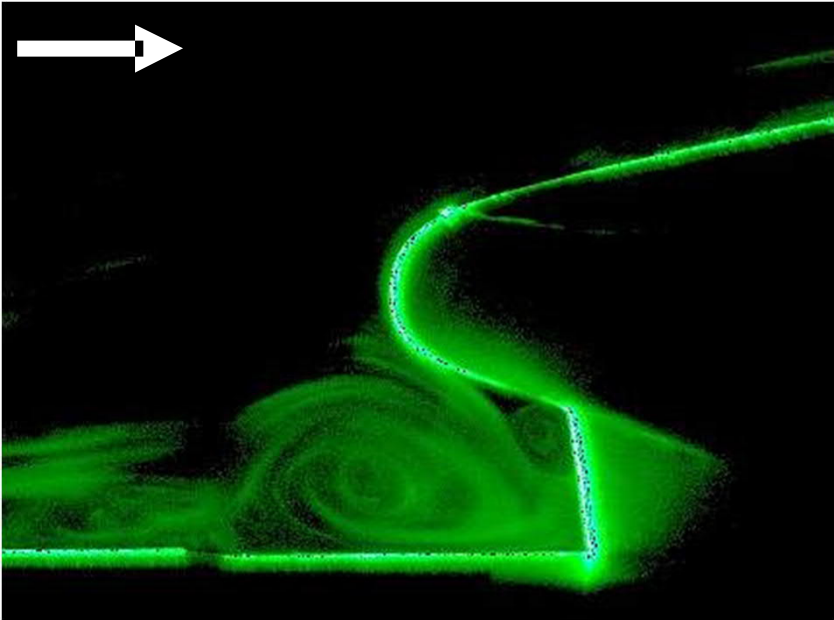


light / laser
sheet
illumination

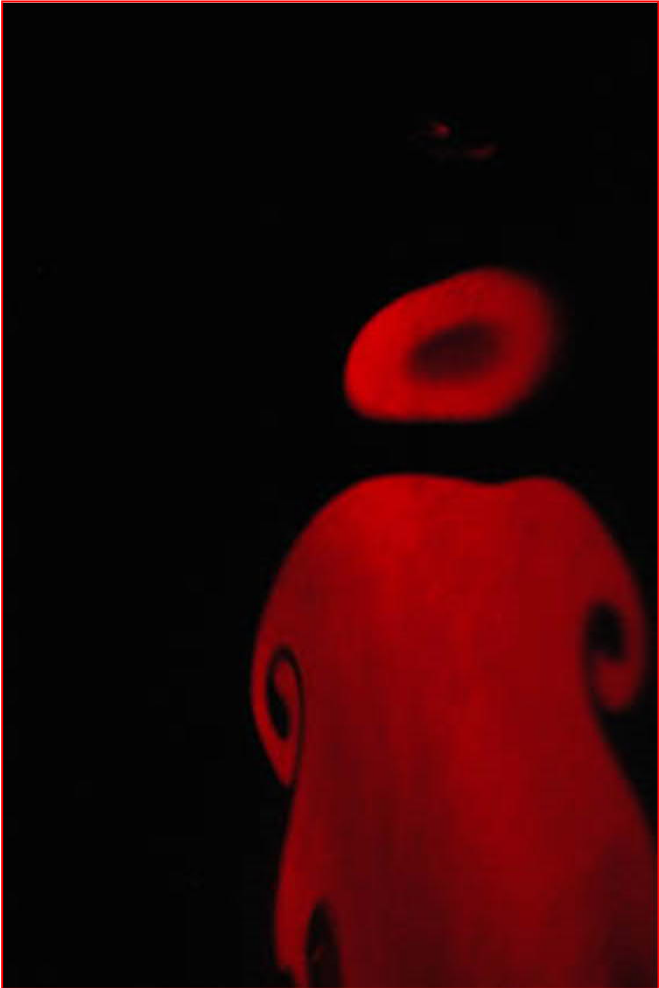
FLOW VISUALIZATION (50 – 100 mW diode)



FLOW VISUALIZATION (50 – 100 mW diode)



FLOW VISUALIZATION
(50 – 100 mW diode)



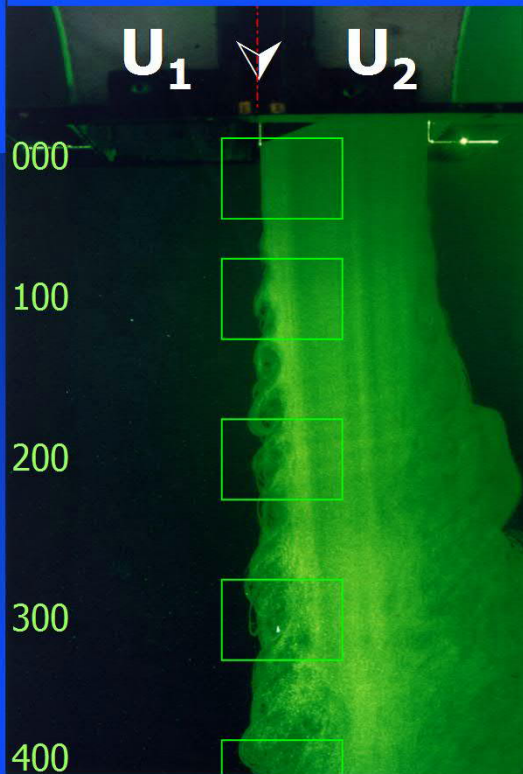
FLOW VISUALIZATION (6W: Nd:YAG, cont. mode)



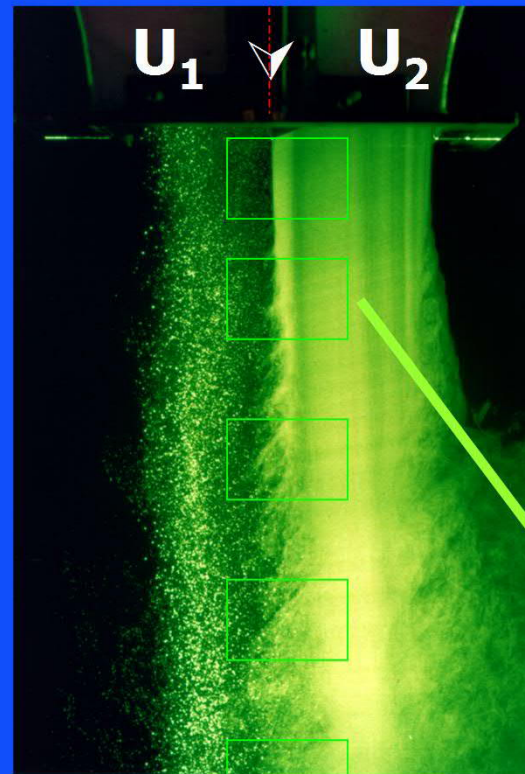
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Final Public Presentation on 26th/06/2000

Single-Phase Flow



Two-Phase Flow



Flow Visualization

$U_1 = 2 \text{ m/s}$
 $U_2 = 1 \text{ m/s}$

Digital Image Recording for Particle Imaging Velocimetry

PIV PTV(S)

Only the low speed, right side jet is seeded with smoke !

500 Mixing Layer Development

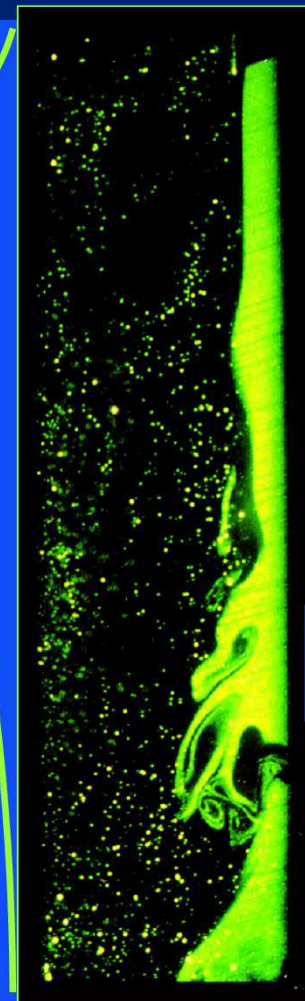
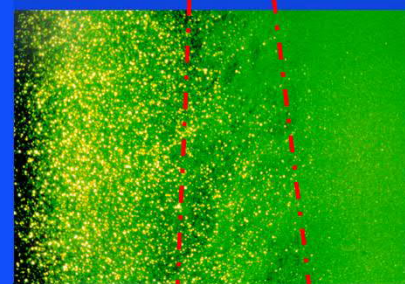
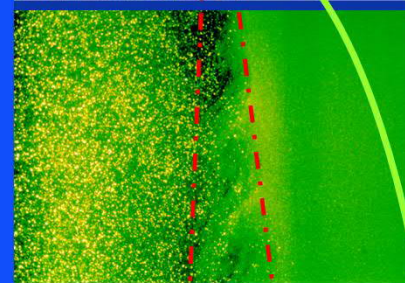
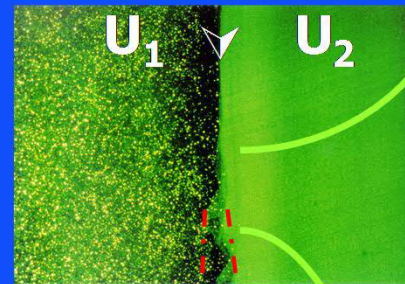
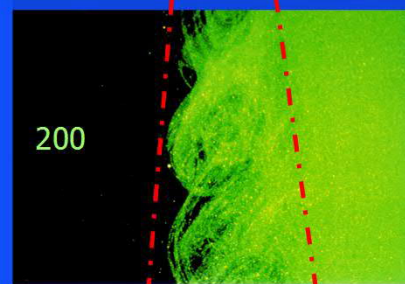
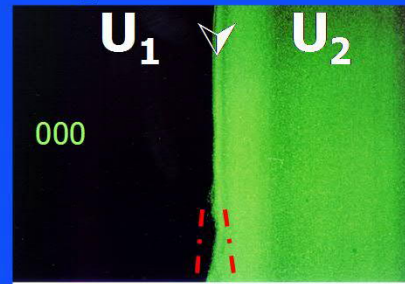
FLOW VISUALIZATION (6W Nd:YAG, cont. mode)



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Single-Phase Flow Two-Phase Flow



**Flow
Visualization**

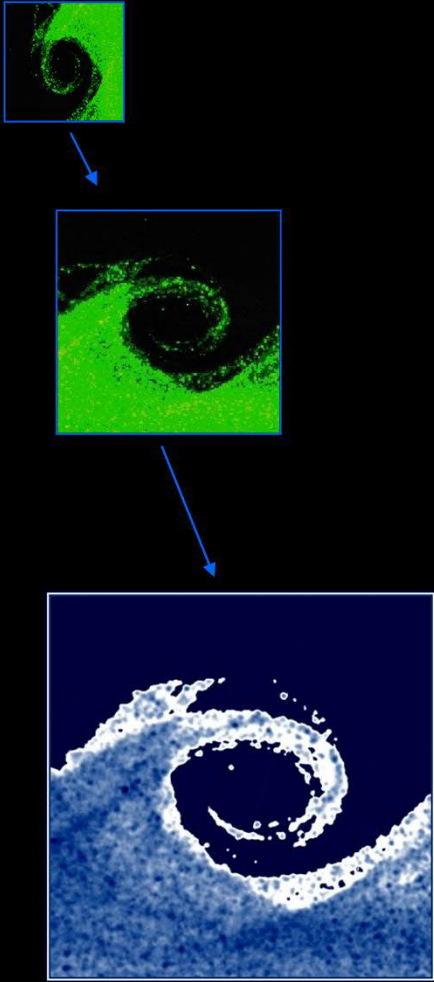
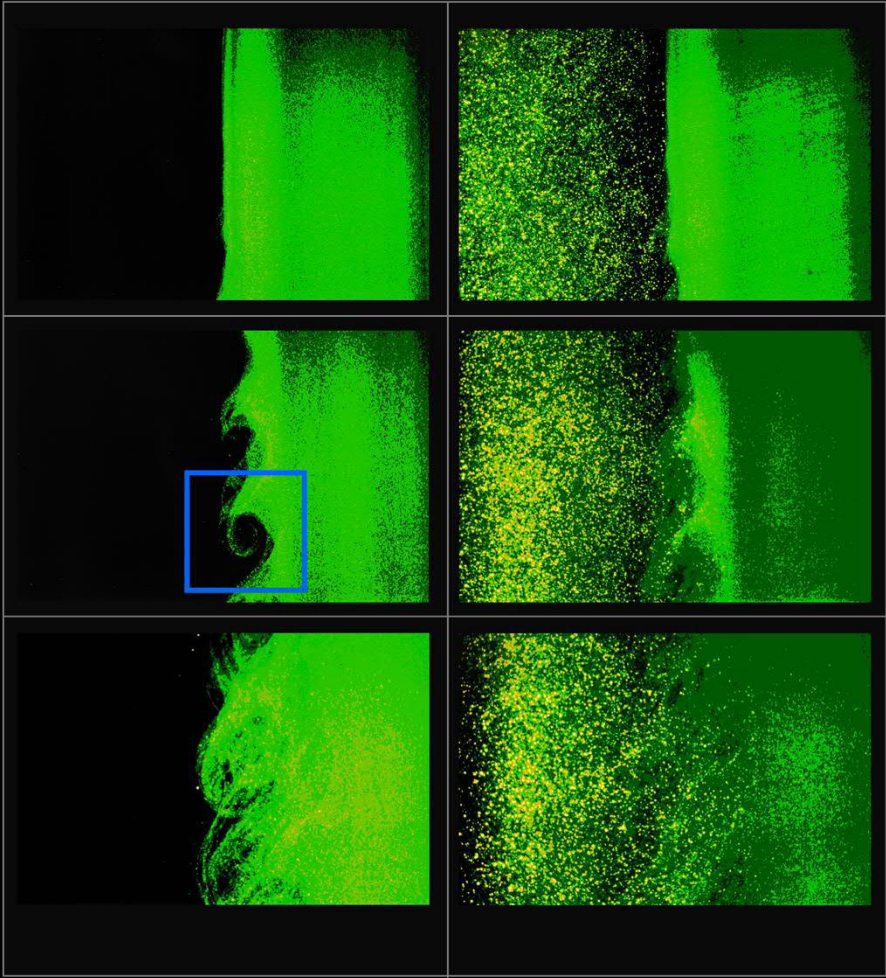
$U_1 = 2 \text{ m/s}$
 $U_2 = 1 \text{ m/s}$

**shear layer
flow structure**

Only the low speed, right side jet is seeded with smoke !

Vorticity Thickness

FLOW VISUALIZATION (6W Nd:YAG, cont. mode)



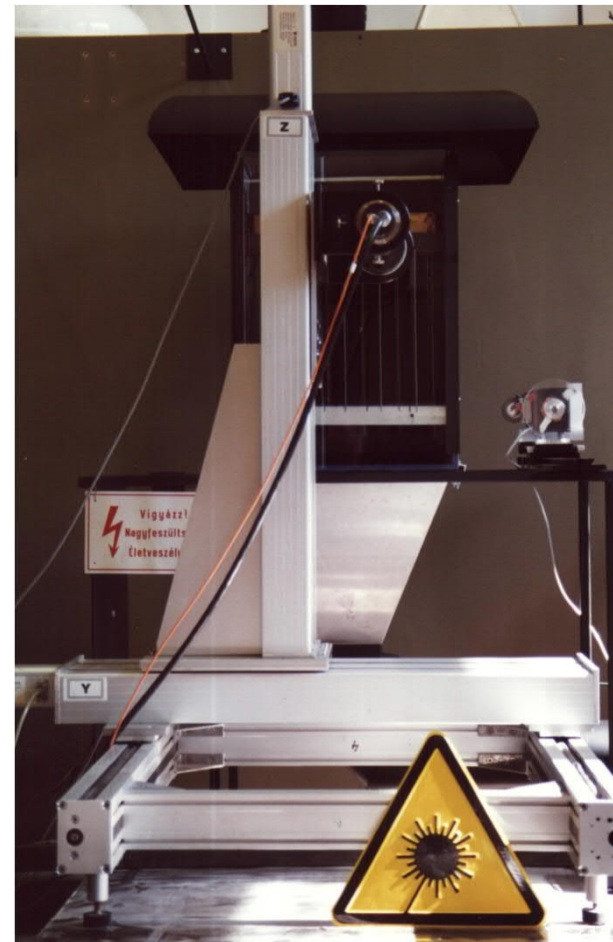
Áramlástan Tanszék

LASER DOPPLER ANEMOMETRY

LDV POLYTEC LDV-380 100mW diode laser
1D: only for single velocity component meas.

$\lambda = 810 \text{ nm}$ (infrared)

(R&D cooperation with UNI MAGDEBURG)



PARTICLES

Types and sizes of particles
BEHAVIOUR in the carrier flow
„seeding / tracer” problematic

Types of „aerosols” $0.01\mu\text{m} < d_p < 50\mu\text{m}$

Dust:

size range: $d \geq 0,2 [\mu\text{m}]$

description: solid particles, produced by breaking or attrition, abrasion, wearing of solid substances, perceptible to the eye, the diameter is larger than the wave length of light.

Smoke (fume):

size range: $d \leq 1 [\mu\text{m}]$

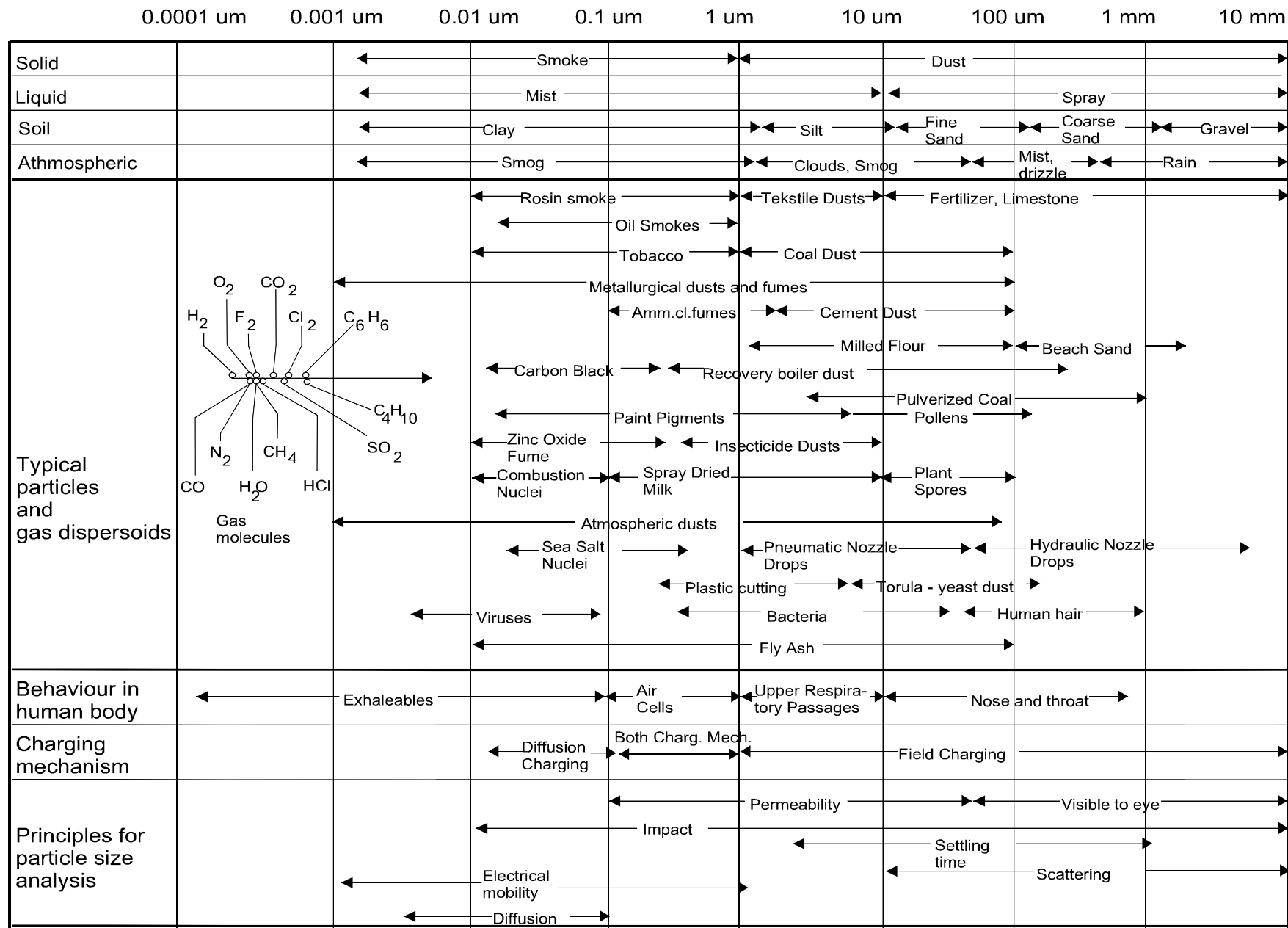
description: solid or liquid particles or droplets, originated from condensation or chemical reaction, in most cases chain-like structures. Produced at combustion, chemical processes etc.

Mist (fog):

size range: $0,1 \leq d \leq 200 [\mu\text{m}]$

description: liquid droplets originated from steam condensation or by atomization, spraying. The mist droplets and the saturated steam of that liquid are in equilibrium state.

PARTICLES



BASIC FUNDAMENTALS OF LIGHT SCATTERING

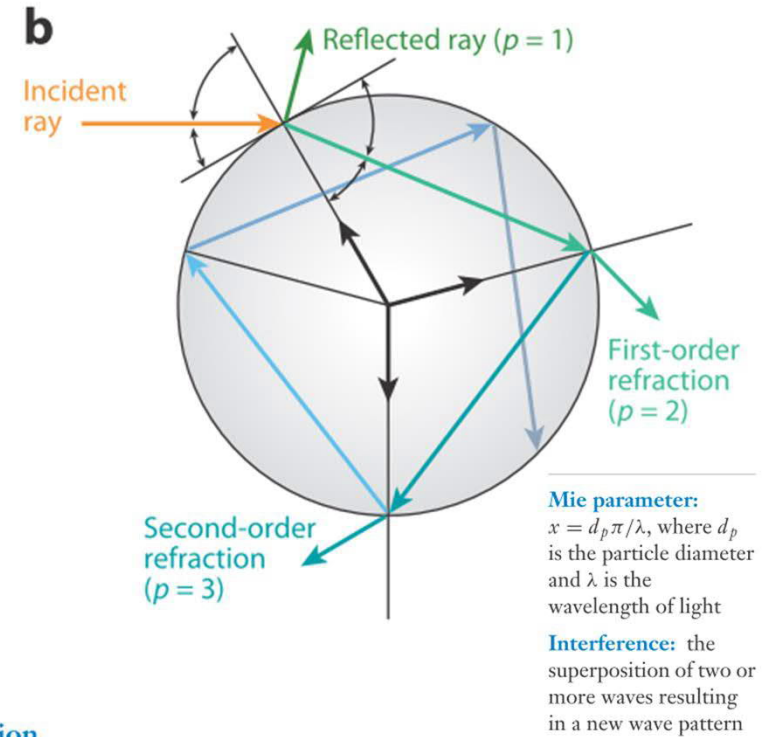
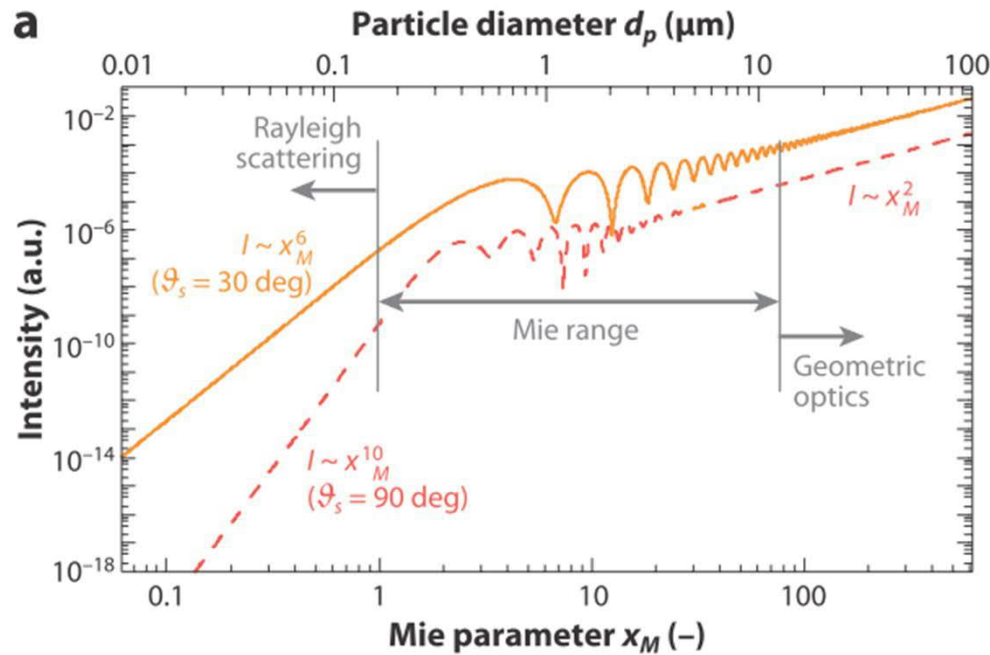


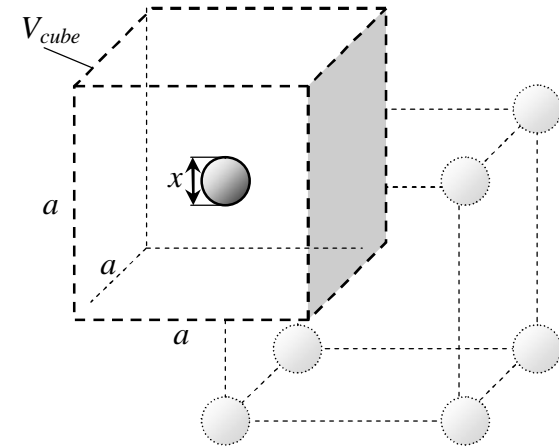
Table 1 Overview of measurement techniques for optical particle characterization

Measurement principle	Measured quantity	Measurement technique
Direct imaging	Velocity, size, shape	PIV/PTV, shadowgraphy, glare-point separation
Intensity, intensity ratio	Size, temperature, species	Extinction/absorption, modulation depth, Mie/LIF ratio, two-band/three-band LIF
Interferometry	Velocity, size, refractive index/temperature	Laser Doppler, phase Doppler, ILIDS/IPI, diffraction, rainbow refractometry, holography
Time shift	Size, velocity	Time of flight, pulse displacement, time-shift technique
Pulse delay	Size, temperature	Femtosecond laser methods
Raman scattering	Temperature, species concentration	Raman spectroscopy

Abbreviations: ILIDS, interferometric laser imaging for droplet size; IPI, interferometric particle imaging; LIF, laser-induced fluorescence; PIV, particle image velocimetry; PTV, particle tracking velocimetry.

PARTICLES

$c[\text{g}/\text{m}^3]$	$\frac{a}{x}$	N [db/cm ³]
10	47	350.000
1	101	35.000
0.1	218	3.500



Let's calculate the c [kg/m³] mass concentration of n particles evenly distributed in a particle-gas mixture having a volume of V_{g+p} . Let's assume that each particle is sitting in the center of a cube. (see Figure below).

The concentration can be calculated:

$$c = \frac{\sum m_p}{V_{g+p}} \cong \frac{\sum m_p}{V_{g+p}} = \frac{\sum V_p \cdot \rho_p}{V_{g+p}} = \frac{n \cdot \frac{x^3 \cdot \pi}{6} \cdot \rho_p}{n \cdot a^3} = \frac{x^3 \cdot \pi}{6} \cdot \rho_p$$

where c [kg/m³] mass concentration, a [m] average distance between particles, ρ_p [kg/m³] density of particles, n is number of particles.

For the average relative distance (a/x) between neighboring particles in gas we get:

$$\frac{a}{x} = \sqrt[3]{\frac{\rho_p \cdot \pi}{6 \cdot c}}$$

Conclusion:

- in case of usual particle concentration values the particle-laden flows are very dilute mixtures. (the distance between neighboring particles is very large).
- particles are present with very high number even in particle-gas mixtures having very low concentration.

PARTICLES (seeding / tracer problematic)

We need to seed, but only with particles that follow (trace) the flow field.

What does it mean: follow the flow?

Inertial parameter: $\Psi_p = St_p$: particle Stokes number

By neglecting the effect of the gravity field strength the dimensionless equation of motion of particles will turn to another form using the w_s settling velocity:

$$\frac{du'}{dt'} = \frac{l_0}{v_0^2} g + \frac{18\mu}{x^2 \rho_p} \frac{l_0}{v_0} \underline{w}' \approx \frac{18\mu}{x^2 \rho_p} \frac{l_0}{v_0} \underline{w}' = \frac{g \cdot l_0}{w_s v_0} \underline{w}'$$

$$\frac{du'}{dt'} = \frac{g \cdot l_0}{w_s v_0} \underline{w}'$$

Introducing ψ inertia parameter will help us to evaluate the particle motion in gas flow:

$$\psi = \frac{w_s v_0}{g \cdot l_0}$$

Dimensionless momentum equation for particles with inertia parameter:

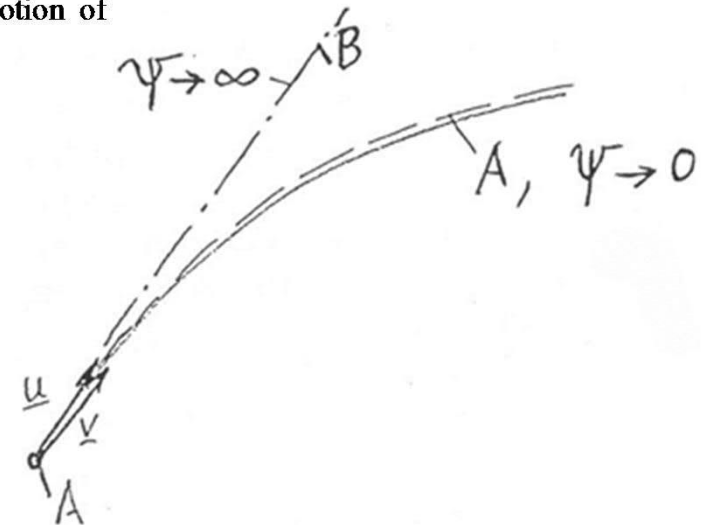
$$\frac{d\underline{u}'}{dt'} = \frac{1}{\psi} \underline{w}' = \frac{1}{\psi} (\underline{v}' - \underline{u}')$$

case A) dashed line in the upper figure

When $\psi \rightarrow 0$, for small (x) and/or light (ρ_p) particles, which settling velocity is small, or $w_s \rightarrow 0$, and if $(\underline{v}' - \underline{u}') \neq 0 \Rightarrow \frac{d\underline{u}'}{dt'} \rightarrow \infty$, hence particle move along the gas streamline, particle follow the carrier gas flow.

case B) dash-dot line in the upper figure

When $\psi \rightarrow \infty$, for large and/or heavy particles, which settling velocity is large, $\frac{1}{\psi} \rightarrow 0$, consequently $\frac{d\underline{u}'}{dt'} \rightarrow 0$. hence particle move along its initial path, leaving the gas streamline.



PARTICLES

Settling velocity of the particle (w_s):Settling of particle of ρ_p density in a gas of ρ_g density:

$$w_s = \frac{x^2(\rho_p - \rho_g)g}{18\mu}$$

Correction of settling velocity due to the diffusion effect in submicron size-range:

$$w_{s,corr} = Cu \cdot w_s$$

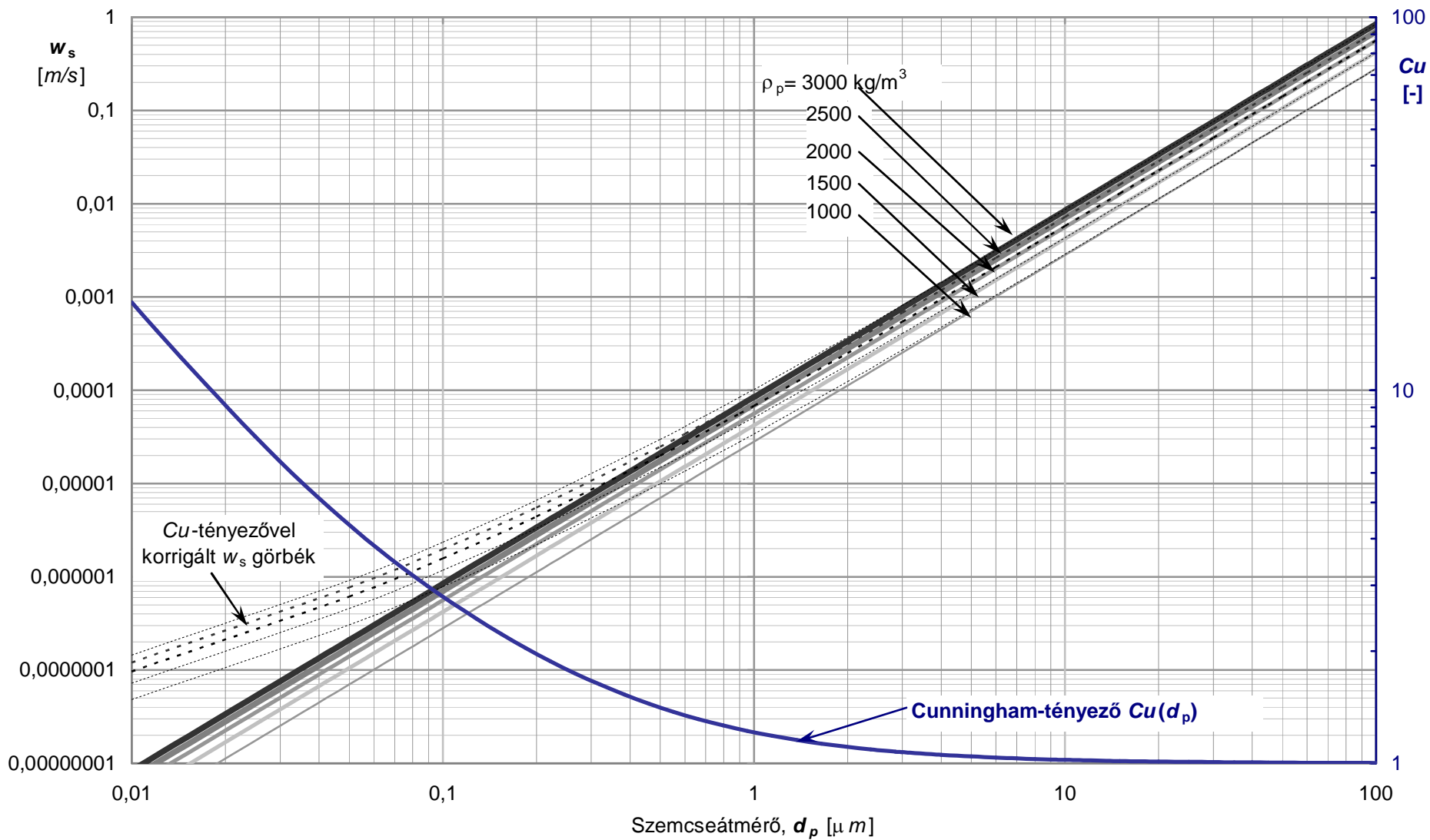
where $Cu = 1 + \frac{2 A \lambda}{x}$ is the Cunningham coefficient (or Cunningham correction factor),

where $A \approx 1.4$, and λ is the mean free path of molecules, at room-temperature $\lambda = 6.5 \cdot 10^{-2} \mu\text{m}$).

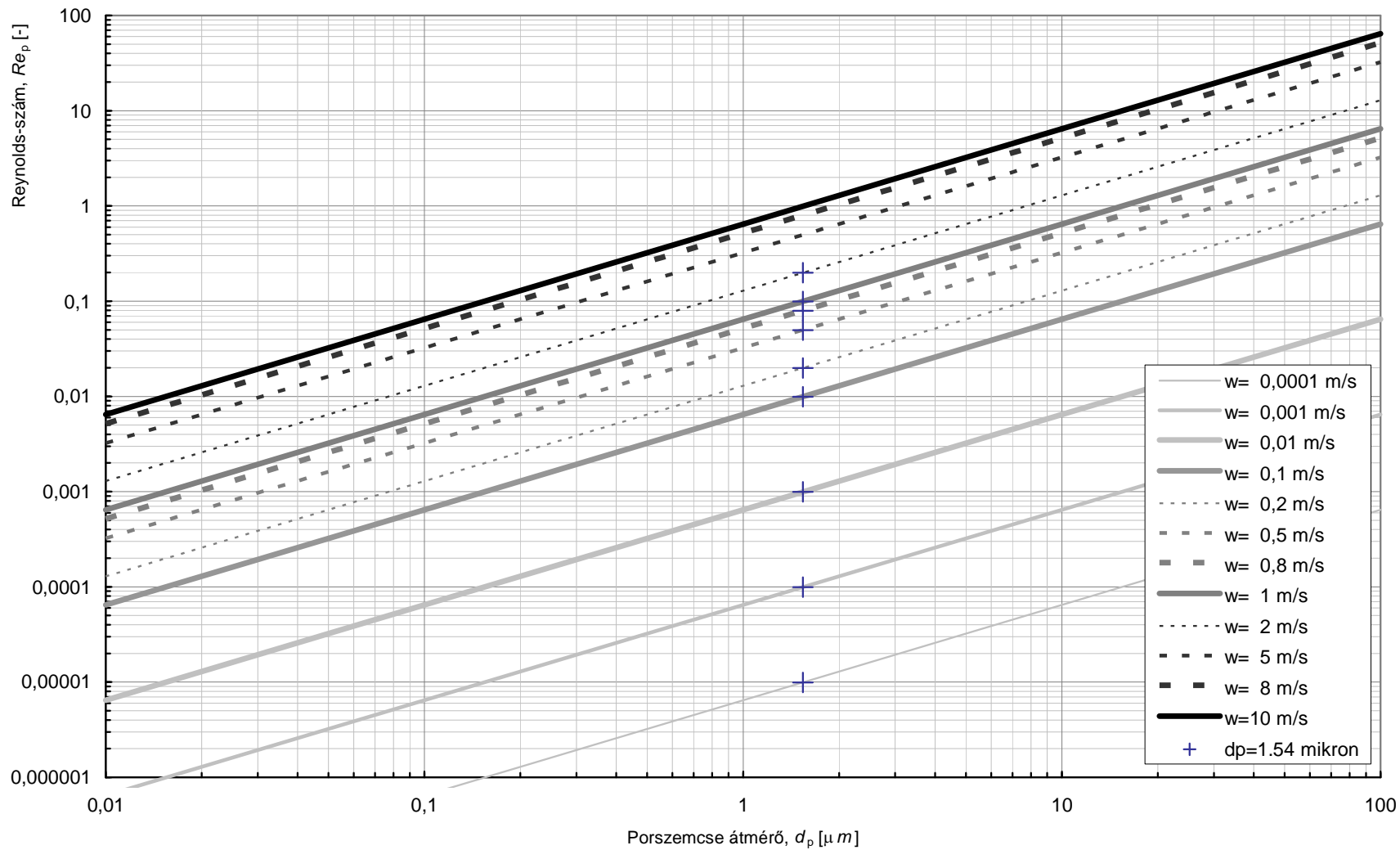
$$Cu = 1 + \frac{2 A \lambda}{x}$$

$$Cu = 1 + 1,246 \cdot \frac{2\lambda}{d_p} + 0,42 \cdot \frac{2\lambda}{d_p} \cdot e^{-0,87 \frac{2\lambda}{d_p}}$$

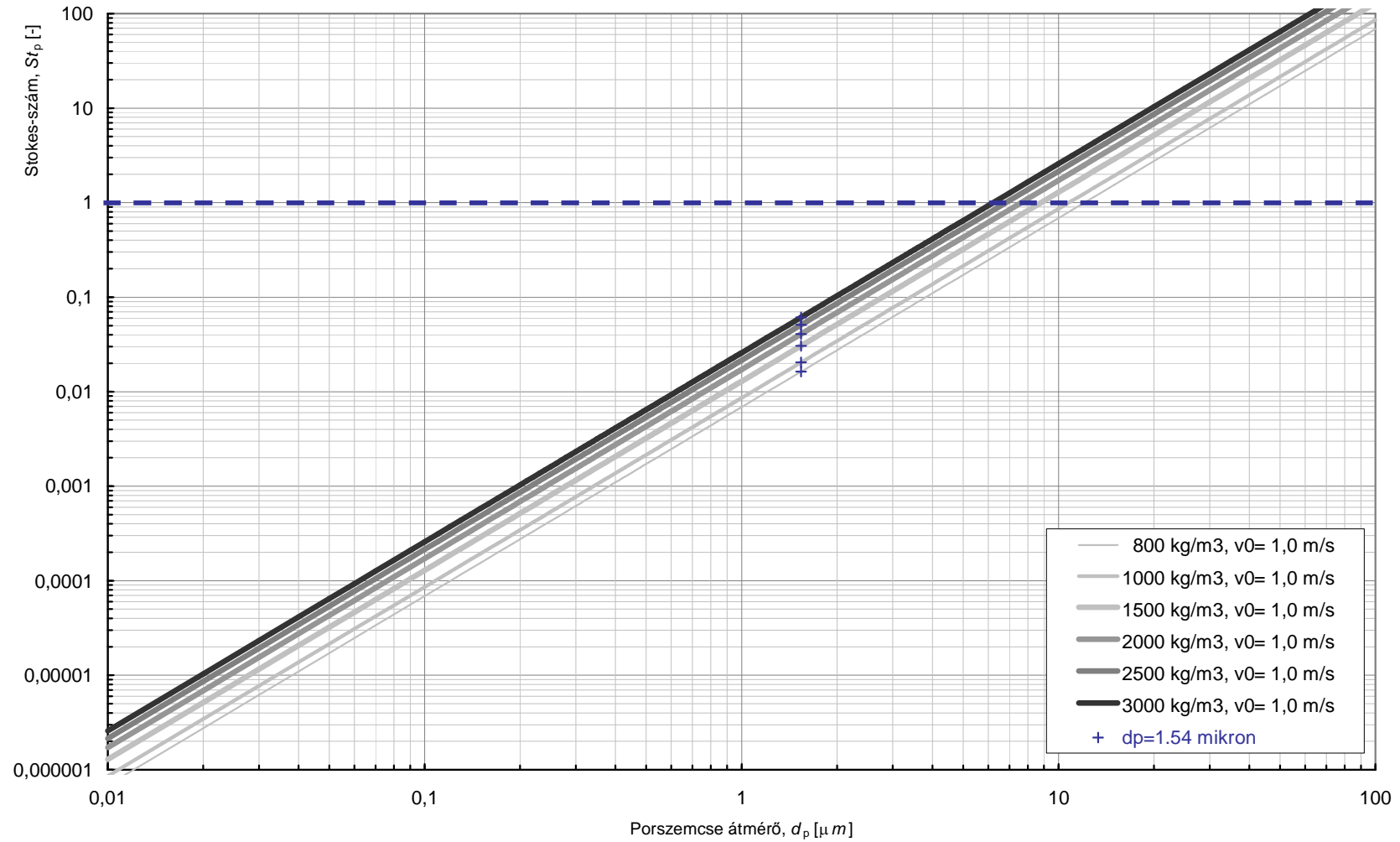
PARTICLES: setting velocity = *function of* (particle diameter)



PARTICLES: particle Reynolds-number = *function of* (particle diameter)



PARTICLES: particle Stokes-number = *function of* (particle diameter)



PARTICLES

Charatceristic parameters of the primary & secondary phase:

- carrier fluid (primary phase)
- seeding /tracer particles (secondary phase)

Volume ratio:

$$\alpha_p = \frac{V_p}{V_g} = \frac{\frac{d_p^3 \pi}{6}}{a^3} = \frac{c_p}{\rho_p}$$

Mass loading ratio:

$$M = \frac{c_p}{\rho_g} = \alpha_p \frac{\rho_p}{\rho_g}$$

$$\frac{M}{\alpha_p} = \frac{\rho_p}{\rho_g}, \text{ or } \frac{\alpha_p}{M} = \frac{\rho_g}{\rho_p}$$

where:

c_p : particle mass concentration

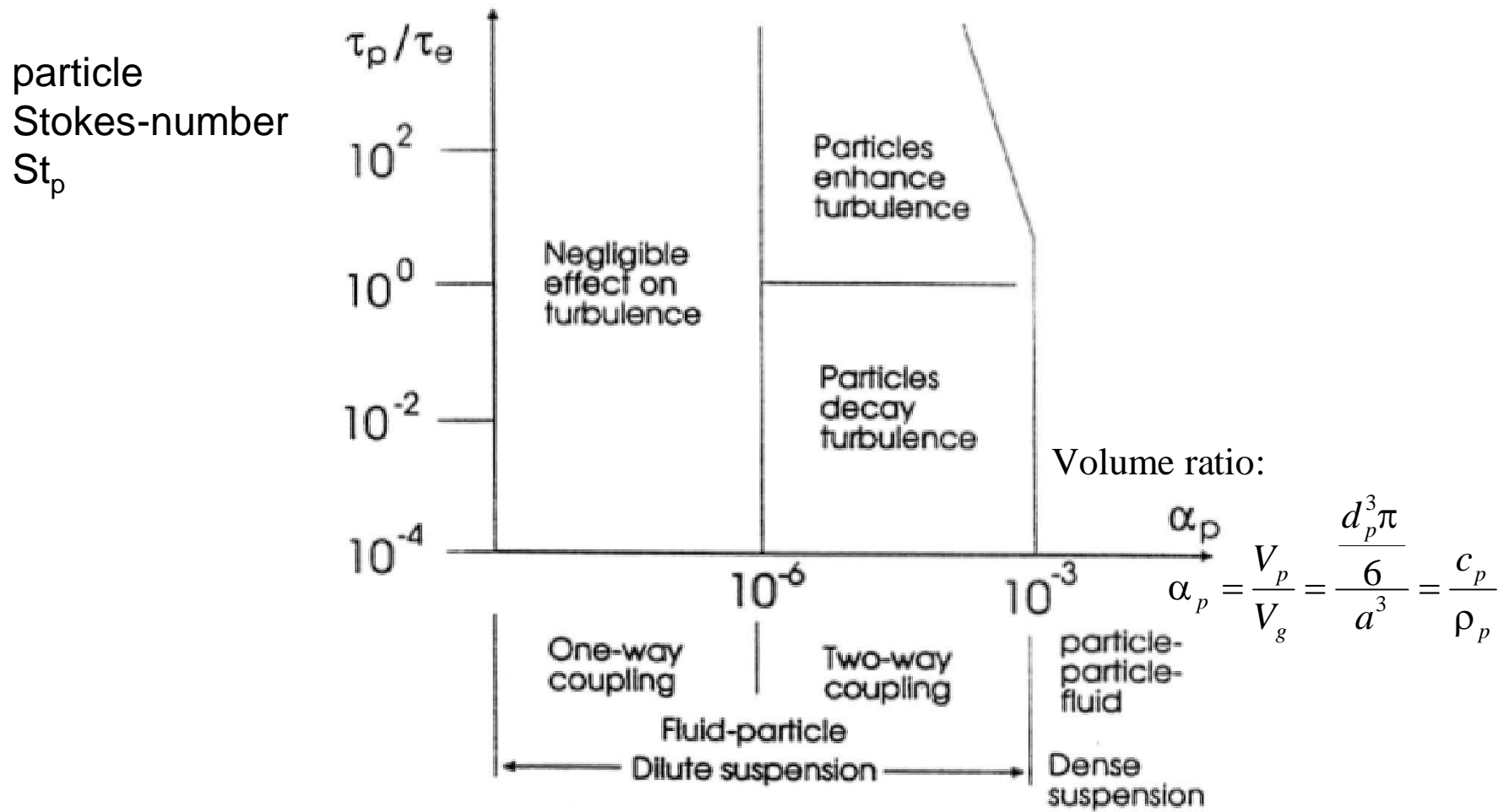
ρ_g : density of gas (carrier phase)

ρ_p : density of particle (material)

α_p		$\rho_p [kg/m^3]$		
		800	1500	2500
$c_p [g/m^3]$	0,0001	$1,3 \cdot 10^{-10}$	$6,7 \cdot 10^{-11}$	$4,0 \cdot 10^{-11}$
	0,001	$1,3 \cdot 10^{-9}$	$6,7 \cdot 10^{-10}$	$4,0 \cdot 10^{-10}$
	0,01	$1,3 \cdot 10^{-8}$	$6,7 \cdot 10^{-9}$	$4,0 \cdot 10^{-9}$
	0,1	$1,3 \cdot 10^{-7}$	$6,7 \cdot 10^{-8}$	$4,0 \cdot 10^{-8}$
	1	$1,3 \cdot 10^{-6}$	$6,7 \cdot 10^{-7}$	$4,0 \cdot 10^{-7}$
	10	$1,3 \cdot 10^{-5}$	$6,7 \cdot 10^{-6}$	$4,0 \cdot 10^{-6}$
	100	$1,3 \cdot 10^{-4}$	$6,7 \cdot 10^{-5}$	$4,0 \cdot 10^{-5}$

M		$\rho_g [kg/m^3]$		
		0,8	1,0	1,2
$c_p [g/m^3]$	0,0001	$1,3 \cdot 10^{-7}$	$1,0 \cdot 10^{-7}$	$8,3 \cdot 10^{-8}$
	0,001	$1,3 \cdot 10^{-6}$	$1,0 \cdot 10^{-6}$	$8,3 \cdot 10^{-7}$
	0,01	$1,3 \cdot 10^{-5}$	$1,0 \cdot 10^{-5}$	$8,3 \cdot 10^{-6}$
	0,1	$1,3 \cdot 10^{-4}$	$1,0 \cdot 10^{-4}$	$8,3 \cdot 10^{-5}$
	1	$1,3 \cdot 10^{-3}$	$1,0 \cdot 10^{-3}$	$8,3 \cdot 10^{-4}$
	10	$1,3 \cdot 10^{-2}$	$1,0 \cdot 10^{-2}$	$8,3 \cdot 10^{-3}$
	100	$1,3 \cdot 10^{-1}$	$1,0 \cdot 10^{-1}$	$8,3 \cdot 10^{-2}$

PARTICLES



ELGHOBASHI (1994): „Turbulence modulation map”: particle STOKES-number ($St_p = \tau_p/\tau_e$) in function of the α_p

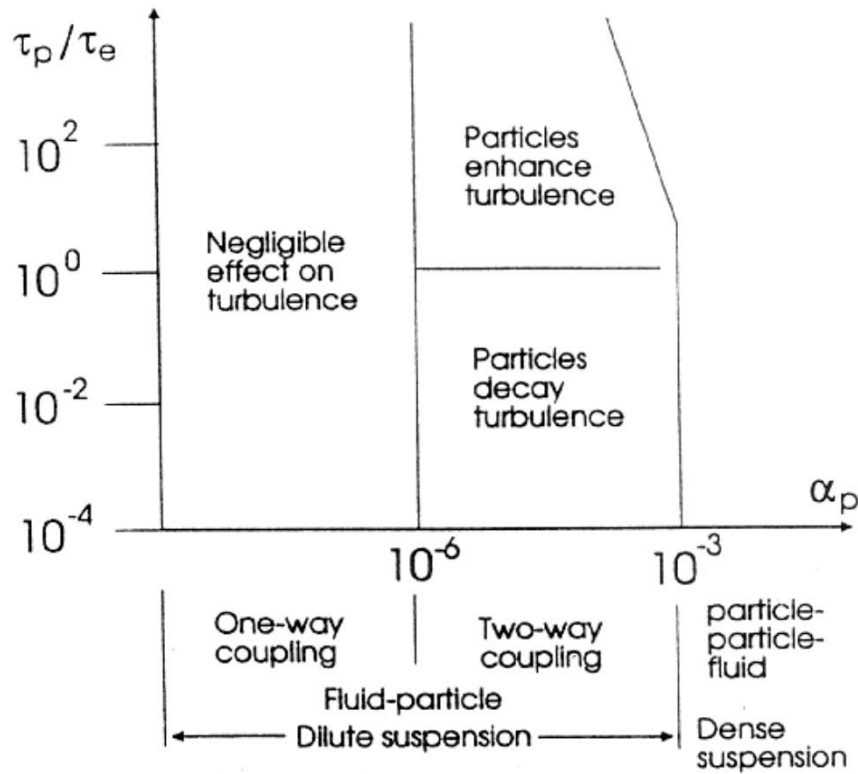
τ_p : characteristic (response) time of the particle

τ_e : characteristic time of the carrier fluid

dilute mixtures: $\alpha_p < 10^{-3}$

dense mixtures: $\alpha_p > 10^{-3}$

PARTICLES' influence on turbulence of the carrier flow



[ELGHOBASHI, 1994]

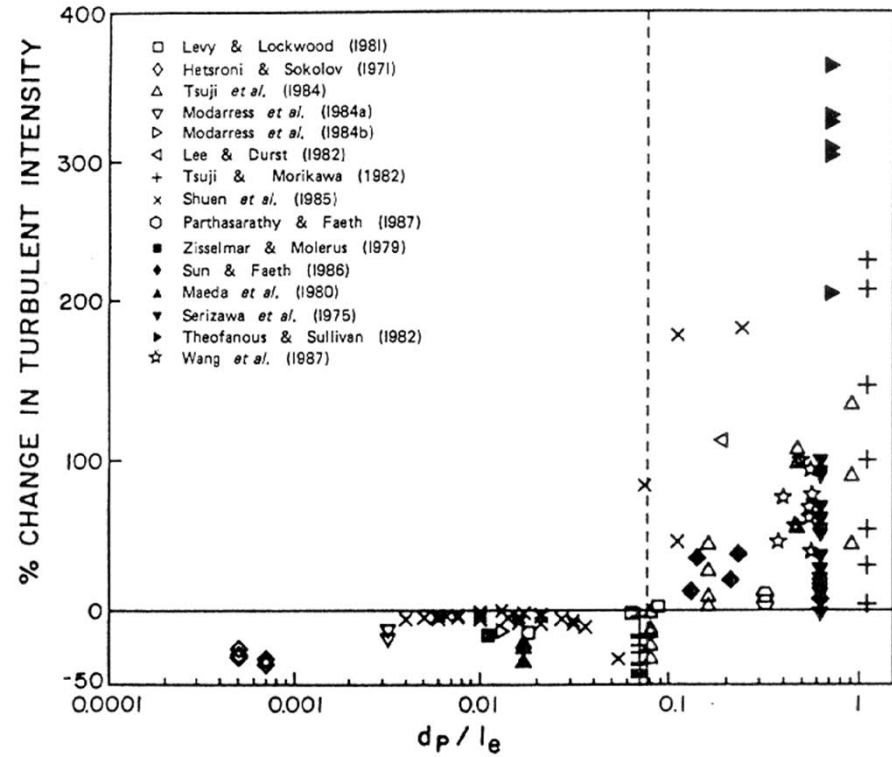


Figure 2. Change in turbulent intensity as function of length scale ratio.

[GORE and CROWE, 1989]

PARTICLES

Table 3. Seeding particles in gas flows.

Material	d_p (μm)	Laser	Pulse energy, pulse time	Light sheet		Reference
				w (mm)	t (mm)	
TiO ₂ ($m = 2.6$, $\rho = 3500 \text{ kg m}^{-3}$)	<1	Nd:YAG	10 mJ, 20 ns	15	0.3	Reuss <i>et al</i> (1989)
TiO ₂ , ZrO ₂	0.7–1	Nd:YAG	110 mJ, 12 ns			Paone <i>et al</i> (1996)
Al ₂ O ₃ ($m = 1.76$, $\rho = 3970 \text{ kg m}^{-3}$)	0.3	Nd:YAG	400 mJ		0.2	Muniz <i>et al</i> (1996)
	3	Nd:YAG	9 mJ, 6 ns			Anderson <i>et al</i> (1996)
	0.8	Ruby	20 ns	150	$\simeq 1$	Krothapalli <i>et al</i> (1996)
Polycrystalline	30	Nd:YAG	135 mJ, 6 ns			Grant <i>et al</i> (1994)
Glass	30	Ruby	30 mJ, 30 ns			Schmidt and Löffler (1993)
Oil smoke	1	Ruby	5 J			Stewart <i>et al</i> (1996)
Corn oil	1–2	Nd:YAG	100 mJ			Jakobsen <i>et al</i> (1994)
Oil	1–2	Nd:YAG	120 mJ		0.4	Westerweel <i>et al</i> (1993)
Olive oil ($m = 1.47$, $\rho = 970 \text{ kg m}^{-3}$)	1.06	Nd:YAG	70 mJ, 16 ns	200	0.5	Höcker and Kompenhans (1991)
						Fischer (1994)
						Raffel <i>et al</i> (1996)

PARTICLES

Table 4. Seeding particles in liquid flows.

Material	d_p (μm)	Laser	CW power or energy, time	Light sheet		Reference
				w (mm)	t (mm)	
TiO ₂	3	Nd:YAG				Longmire and Alahyari (1994)
Al ₂ O ₃	9.5	Ruby	2 J, 30 ns	100	0.8	Liu <i>et al</i> (1991)
Conifer pollen ($\rho = 1000 \text{ kg m}^{-3}$)	50–60	Ar ion	1–2 W			Westergaard <i>et al</i> (1993) McCluskey <i>et al</i> (1995) Gallagher and McEwan (1996)
Polymer ($\rho = 1030 \text{ kg m}^{-3}$)	30	Ar ion	0.5–5 W		0.5	Draad and Westerweel (1996) McCluskey <i>et al</i> (1996)
Phosphorescent polymer	80	Ar ion	5 W		1	Willert and Gharib (1991)
Fluorescent	50	Nd:YAG				Hart (1996)
	20	Cu vapour	45 W		1	Roth <i>et al</i> (1995)
Polystyrene ($\rho = 1050 \text{ kg m}^{-3}$)	500					Khoo <i>et al</i> (1992)
	15	Ruby	25 mJ, 20 ns			Zhang <i>et al</i> (1996)
Thermoplastic ($\rho = 1020 \text{ kg m}^{-3}$)	6	Nd:YAG		50	2	Hassan <i>et al</i> (1994)
Reflective ($\rho = 1010 \text{ kg m}^{-3}$)	60	Ar ion	18 W			Grant <i>et al</i> (1992)
	30	Ar ion	12–18 W	200		Grant and Wang (1994)
Metallic coated	4	Ar ion	2 W		2	Magness <i>et al</i> (1993)
	14	Ar ion			1	Johari <i>et al</i> (1996)
Microspheres ($\rho = 700 \text{ kg m}^{-3}$)	<30	Ar ion				Graham and Soria (1994)
H ₂ bubbles		Ar ion	1 W		0.3	Dieter <i>et al</i> (1994)

PARTICLES

Table 2. Particle response in turbulent flow ($\eta = 0.99$).

Particle	ρ_p (kg m ⁻³)	Gas (10 ⁵ Pa)	Density ratio s	Viscosity ν (m ² s ⁻¹)	f_c (kHz)	Sk_c	d_p (μ m)
TiO ₂	3500	Air (300 K)	2950	1.50×10^{-5}	1	0.0295	1.44
					10		0.45
Al ₂ O ₃	3970	Flame (1800 K)	20250	3.00×10^{-4}	1	0.0113	2.46
					10		0.78
Glass	2600	Air (300 K)	2190	1.50×10^{-5}	1	0.0342	1.67
					10		0.53
Olive oil	970	Air (220 K)	617	1.45×10^{-5}	1	0.0645	3.09
					10		0.98
Microballoon	100	Air (300 K)	84.5	1.50×10^{-5}	1	0.1742	8.50
					10		2.69

the Stokes number Sk , a characteristic non-dimensional frequency of the particle response. Sk is defined here as

$$Sk = \left(\frac{\omega}{\nu}\right)^{1/2} d_p \quad (6)$$

SEPARATE SLIDES!

1. LDA (ppt, Dantec)
2. PIV (ppt, VKI) + Stereo PIV (Dantec)
3. PTV(S) (ppt, PDF, VKI – pivneta course)

Suggested hadout, books, literatures:

Website of Dept. Fluid Mech for this subject:

<http://www.ara.bme.hu/oktatas/tantargy/NEPTUN/BMEGEATMW03/2011-2012-II/>

Springer Handbook of Experimental Fluid Mechanics

(Eds.: Tropea, Yarin, Foss), ISBN 978-3-540-25141-5 (Springer-Verlag Berlin 2007)

Measurement Techniques in Fluid Dynamics – An Introduction

(VKI Lecture Series 2001)

Advanced measurement techniques

(VKI Lecture Series, 1998.)

Optical velocity measurements

(VKI Lecture Series 1994.)

Laser Doppler Velocimetry

(Dantec website: www.dantecdynamics.com)

Particle Image Velocimetry - A Practical Guide

(Eds.: Raffel/Willart/Kompenhans) Springer-Verlag, Berlin 1998, ISBN 978-3-540-72307-3

Flow Visualization - Techniques and Examples

(Eds.: Smits&Lim), Imperial College Press, London, 2003

Laser Doppler and Phase Doppler Measurement Techniques

(Albrecht, Damaschke, Borys, Tropea: Springer-Verlag)

Laser Techniques and Applications in Fluid Mechanics

(Springer Verlag ISBN 3-540-56879-4)

Speckle Metrology (Eds: R.S. Sirohi, , Marcel Dekker, New York, 1993, ISBN 0-82478-932-6

Holographic Interferometry: Principles and Methods

(Kreis) Akademie Verlag, 1996, ISBN 3-05501-644-0

Handbook of Holographic Interferometry

(Kreis) Wiley-VCH, Weinheim 2005, ISBN 3-527-40546-1

Optical Measurement Techniques and Applications

(Ed. Pramod K. Rastogi); Artech House 1997, ISBN 0-89006-516-0

PIV systems:

conventional 2D PIV

stereo PIV

High speed (Time Resolved) PIV

micro PIV

ABILITY of the various systems:

- 2D / Planar system provides velocity measurement in a single plane, normally at frame rates up to 15 image pairs/second.
- Stereo / 3D systems use a pair of cameras to provide stereo / 3D measurement of velocity.
- High speed / time resolved products use high speed cameras and high repetition rate, double pulse lasers to take thousands of image pairs per second to provide time resolved velocity data.
- Micro systems view via a time resolved system and provide flow measurement in microfluidic devices.



CVL: Copper vapour laser

-ideal for high-speed, high-power imaging laser. (short pulse, high beam quality, high power beam) makes it ideal for imaging applications at frequencies 10kHz requiring light-sheets or area illumination.

Applications

- High Speed Imaging
- Time Resolved PIV
- Spray Pattern Measurement
- Flow Visualisation



Specifications:

Laser Type: Copper Vapour Laser

Average Power: 20-35W (depending on model)

Pulse Duration: 25ns

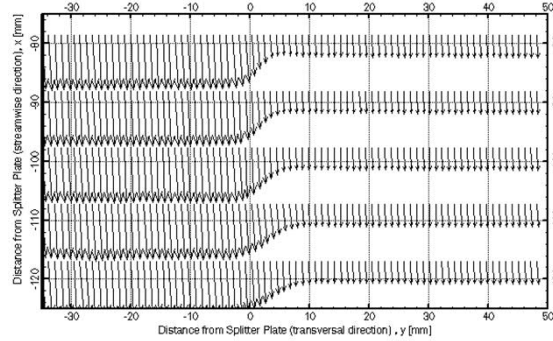
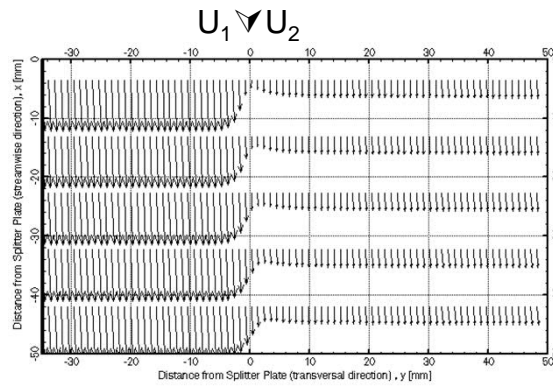
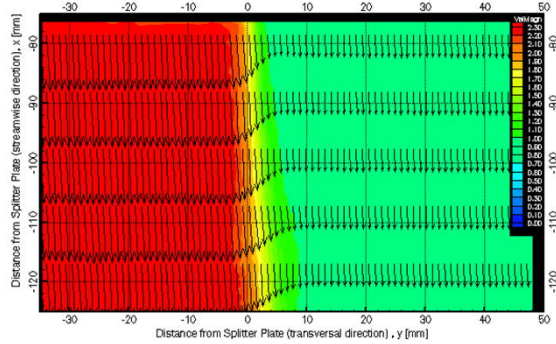
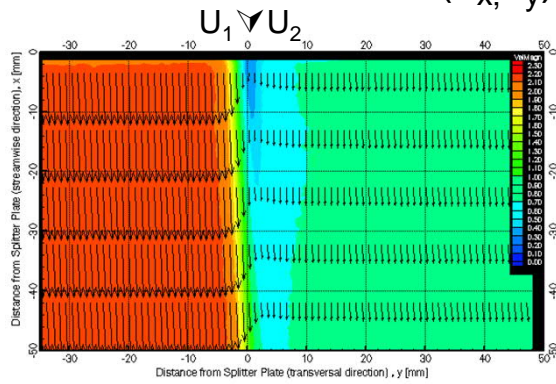
Wavelength: 511nm

Frequency: 3.5-20KHz continuous running frequency. Burst mode frequencies from 0 to 50KHz available.

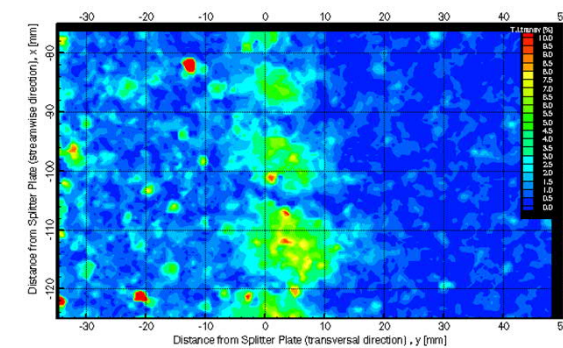
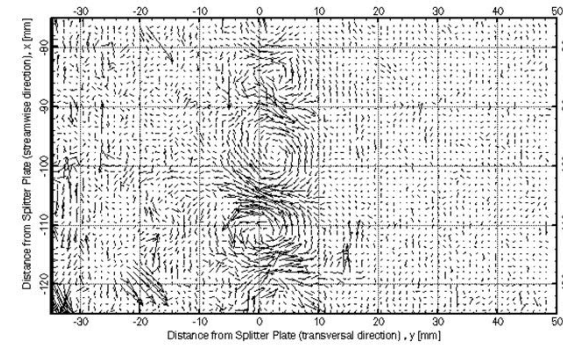
Timing Jitter: <2-5ns (depending on model)

PIV

Instantaneous mean ($v_x; v_y$)



Instant. fluct.
($v'_x; v'_y$)



(transversal T.I.y)